Optimum Fermentation Investigation for PHA Production by

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Abstract

In the universal context where an increasing concern about the nature around us, replacing polymers from petroleum contents with bio-plastics has adversely influenced the stability of the ecosystem. In dead, these bio-plastics have failed to meet the economic thresholds and technical constraints. The only promising and ever studied bio-plastic across all level to date refers to the polyhydroxyalkanoate (PHA). To circumvent related financial issues of PHA, one crucial step is paramount. This is general productivity enhancement and medium nutritional improvement based on the microorganism which produces the biopolymer. Thus, attempts from many nutrition media, have tried to supplement the same with rational sodium glutamate, which underwent tests for development. However, the DSM 545 Cupriavidus necator that produces PHA adequately strained. Media and Luria broth perfect the only efficient producers of the PHA and biomass although a portion of sodium glutamate was used to supplement each respectively. Hence the production level increased by thirty-three times over the original value as compared to the traditional cultivation methods. As a result, PHA through a new route opened by the C. necator appeared more fantastic and suitable with unlimited factors on the medium, rich and enriched substances.

Introduction

Polymers originating from petrochemical have been used as substitutes of other many materials such as metal and glass. Poor disposal amidst excessive use has contributed abundantly to the environmental degradations. Besides, several alternatives have been researched with the result explaining the possible production of polymers which can quickly rot, environmentally friendly. Polyhydroxyalkanoates (PHA) represents the non-toxic, biocompatible, and the biodegradable polymers, replacing several polymers derived from petroleum. Poly is the best of all PHAs; this is because of its mechanical traits and thermoplastic nature. It is a replica of polypropylene. The synthesis of this biopolymer in did through a potential microbial pathway with the use of bacterium Cupriavidus necator. The bacterium is studied widely because its dry mass can be stored up to seventy percent. Different substrates can also be used with the carbon sources.

Additionally, the production of P (3HB) occurs in two distinct phases. Phase one is the growth phase and has all the nutrients needed whereas phase two is the production phase. In period two, the production phase, one essential nutrient has limitations over other carbon sources. The operation and control cost of this bioreactor among other processing downfalls make the commercial competition of this polymer flop when compared to other polymers derived from petroleum. However, this low production will be used as a catalyst in the future polymer commercialization.

Interestingly, reducing the production costs requires an explicit alternative to acting as a supplement in the production of PHA. The proposed agents destabilize the metabolic pathway resulting in higher productivity in cell production, although possibilities are made for PHA direct synthesis. The culture medium supplementation using acetic and propionic acid underwent assessment for proper culture productions in the presence of Cupriavidus necator. PHB is water and ultraviolet radiation resistant. It does not allow oxygen to pass through easily

thus preferable for food packaging. Moreover, it can be used in the sutures surgical with further

development being worked on for excellent application in the future. In its more extensive use, PHB needs cheap products thereby improving strategies in the fermentation and downstream discovery techniques.

Methodology

a. Typical, carbon and salt sources

Caproic, butyric, propionic, fructose and acetic acids, E2 common mineral salts and Standards, salts and carbon sources and poly from Sigma Aldrich were purchased (Albuquerque, Eiroa, Torres, Nunes and Reis, 2007, p. 775). Additionally, an OMCAcid and a dephenolized OMW were employed to stream the anaerobic acidogenic products for the immobilized cells in the laboratories to obtain volatile fatty acids. In the latter stream, volatile fatty acids were produced in different short chains such as (g/l); valeric (0.2), Propionic (1.4), acid (6) among others. In filtering OMWAcid and OMWDeph, a social media is formed. Similarly, dissolving the equal amount of ammonia-free salts in the prepared OMWDeph and the latter OMWAcid in a sterilized autoclave plus centrifugation performance, a purified solution which is clear is formed.

b. The Extraction of the Biopolymer

The extraction of the biopolymer was carried out by a developed method purposely to outline the actual polyester amount used in the process. About six mL broth cultures were acted upon for thirty minutes to produce a solution of acidified methanol and chloroform in a five-milliliter solution respectively. After series of the solution heating, a residue of the cell pellet remained for three hours under optimum room temperature. Later, a solution of three phases was observed from the process.

c. Inoculum and Bacterial Strain

In the DSMS 545 Cupriavidus necator, inoculum originated from a twenty-four-hour growing plate of LB-Agar. Within a day, a significant improvement in quantity and temperature was evident from the LBErlenmeyer flask. The condition of incubation was marked at 150RPM and 30°C respectively.

d. Analytical Approaches

The sampling of data was done periodically. Cary-100 was used to measure optical density whereas spectrophotometer was designed variation detection in the cellular concentration. An OD determines the cellular levels which are based on the cell dry weight. Besides, the obtained sample undergoes centrifugation, separating the pellet and supernatant for future stock analysis (Koller, Hesse, Bona, Kutschera, Atlić and Braunegg, 2007, p. 840). However, the study of fructose was done by implication of an H column of Varian Hi-Plex in an HPLC-IR analysis leaving sulfuric acid to be the only mobile phase. Additionally, the PHAs determination depended on the CB column description by methanolysis method using temperature. Thermogravimetric analysis method was used to ascertain the validity of the analytical method.

e. The Experimental approach

For the success of C. necator, OMWDeph was used as a solvent. The E2 common mineral was prepared by balancing growth of different experiments in distilled water and relatively small proportions of OMWDeph for maximum volume determination under minimal effects inhibitions

(Pantazaki, Papaneophytou, Pritsa, Liakopoulou and Kyriakidis, 2009, p. 860). To achieve these different five conditions were tested to verify the OMWDeph percentage used for the culture medium preparation. Similarly, a description of the previous incubation conditions was done under inoculating distinguished batch test to produce a balanced growth within twenty-four hours. Later, it took six minutes to attest the end of the growth phase. Besides, the resurgence of accumulation phase re-suspended the pellet collections which were used to represent PHA.

f. The measurement of Cell Dry Weight

The absorbance rate of the cell dry weight from the cell optical density measurement indicates a higher price with the spectrophotometer measure of wavelength. This is after slight dilution of the dry cells in distilled water. Later, the determination of CDW was done concerning the calibration standard curve; where CDW function as the only pure culture of the rest of other medium cultures of the microorganism.

Proposed Outcome and Results

The growth results from the inhibition test show that culture media preparation with only distilled experiences maximum absorption of OMWDeph and 3.75 A.U. similarly, a 3.66 A.U was the final OD condition which can be extracted from the result of the control experiments be carried out before. This was treatment from olive mill 99 of wastewater condition in the production of PHA by the Cupriavidus necator.

Alternatively, an observation of the potent inhibition of culture medium was evident containing approximately 60% of OMW (Rodríguez, Koller, Miranda, Calafell–Monfort,

Braunegg, and Marqués, 2013, p. 1337). On the other hand, after eighty hours 60% OMWDeph related experiment was observed concerning the OD within the same exponential rate as discussed before (Patwardhan and Srivastava, 2008, p.177). Further explanation revealed that employed strains must have a specific cell concentration which is an equivalent to 0.5 (A.U) of OD. This represents the rich exponential present in the inhibitors. Particularly polyphenols can be used to inhibit growth because almost 1 g/L phenols exist in the dephenolized wastewater.

Additionally,

The PHA feasibility test productions in the OMWAcid accumulate a significant detection in the growth trend. Interestingly, the growth was found to be possible even without the polyphenol inhibitions. Indeed, both conditions can be used as a representative because the final production of PHA content is scarce and low in productivity thus delaying the feasible biotechnological industrial process.

Conclusion

The carbon sources have unique effects surrounding the biopolymer. The molasses, fructose, and whey in the PHB production passed through a subsequent investigation for an extensive analysis. The four species; A. lata DSMZ 1123, H. pseduflava DSMZ 1034, A. beijinckii DSMAZ 1041, and C.necator DSMZ 545 were measured to determine the quantity of PHB produced from the mixture in the experiment. The maximum concentration of the biopolymer was determined in 60g.L of carbon source concentration and 6 g/L from the corresponding biomass concentration. Fructose and C. necator DSMZ 545 in the biomass

concentration ensure summation of PHB in the PHA to a maximum production rate. In a generation the masses, approximately eighty hours is needed from the beginning of the growth process. Using the Leudeking -piret model it was realized that PHB obeys kinetic production based growth. Relatively 30°C of temperature were obtained plus a shaking rate from the four experimented species. However, PHB recorded a maximum accumulation after fifteen hours from the beginning of the growth. Further results from the surface response analysis show that PHB production can function from dry cell weight.

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